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- (56) References cited: EP-A- 0 156 464

US-A- 3 494 897

### Description

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This invention relates to a novel random copolymer comprising at least polymerized units from ethylene and polymerized units from a cycloolefin as monomers, and a process for production thereof. More specifically, it relates to a cycloolefin type random copolymer having excellent transparency, thermal resistance, heat aging resistance, chemical resistance, solvent resistance, dielectric properties and mechanical properties and a narrow molecular weight distribution.

Polycarbonate, poly(methyl methacrylate) and poly(ethylene terephthalate) are known as synthetic resins having excellent transparency. The polycarbonate resin has excellent heat resistance, heat aging resistance and impact strength as well as excellent transparency, but have the defect of poor chemical resistance since it is readily attacked by strong alkalis. Poly(methyl methacrylate) has the defect that it is susceptible to attack by ethyl acetate, acetone and toluene, is swollen in ether, and has low heat resistance. Polyethylene terephthalate has excellent heat resistance and mechanical properties but has the defect of possessing weak resistance to strong acids or alkalis and of being susceptible to hydrolysis.

Many polyolefins well known as general-purpose resins have excellent chemical resistance, solvent resistance and mechanical properties, but have poor heat resistance. Furthermore, they have poor transparency because they are crystalline. The transparency of polyolefins is generally improved by adding a nucleating agent to render the crystal structure fine, or by performing quenching to stop the growth of crystalls, but such measures have not proved to be entirely effective. Rather, the addition of a third component such as the nucleating agent is likely to impair the inherent excellent properties of the polyolefins. Furthermore, the quenching method requires large scale equipment, and is also likely to reduce heat resistance or rigidity with a decrease in crystallinity.

On the other hand, methods have been proposed for producing polymers having superior transparency by copolymerizing ethylene with bulky comonomers. U.S. Patent 2,883,372 discloses a copolymer of ethylene with 2,3-dihydrodicyclopentadiene. This copolymer has a well balanced combination of rigidity and transparency but low heat resistance as shown by its glass transition temperature of about 100°C.

Japanese Patent Publication No. 14,910/1971 discloses a process for producing a homo- or co-polymer having polymerized units represented by the following formula (a)

wherein R is hydrogen or a lower alkyl group, which comprises polymerizing a 1,4,5.8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene represented by the following formula (b)

wherein R is as defined above,

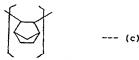
alone or with a cyclic olefin selected from styrene, acenaphthylene, bicyclo-[2.2.1]heptene-2, alkyl-substituted products of the heptene and cyclopentene in the presence of an alcohol as a reducing agent using a halide of a noble metal such as ruthenium as a catalyst.

Homo- or co-polymers comprising the 1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene as part or the whole of monomers and methods for production thereof are also disclosed in Japanese Laid-Open Patent Publications Nos. 159,598/1975, 127,728/1983, 51,911/1984, 81,315/1984 and 81,316/1984 and U. S. Patent 4,178,424.

The polymers disclosed in these prior art documents are ring-opened polymers having polymerized units resulting from ring-opening of monomers as in the polymerized units represented by formula (a). As can be understood from formula (a), these ring-opened polymers are structurally characterized by the fact that the main polymer chain contains an unsaturated vinyl linkage. Because of the presence of the unsaturated vinyl linkage, these polymers have poor heat aging resistance.

All of the polymers described in the above prior art documents are ring-opened polymers obtained by the ring scission of a monomer. U. S. Patents 3,330,815 and 3,494,897 and Journal of Polymer Science: Polymer Physics Edition, volume 12, 1607-1618 (1974) describe polymers of the type obtained by the opening of the double bond of a monomer without the ring scission of the bicyclohepit2-ene skeleton of the monomer.

U. S. Patent 3,330,815 discloses that a polymer comprising polymerized units of the following formula (c)



or the substitution product thereof is obtained from bicyclo[2.2.1]hept-2-ene -2-ene of the following formula (d)

or its substitution product.

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 $U. S. \ Patent 3,494,897 \ discloses \ a process for producing a copolymer of ethylene \ with a \ bicyclo(2.2.1]-hept-2-ene represented by the following formula (e)$ 

Example 44 and claim 92 of this patent discloses a copolymer of ethylene with tetracyclo[6,2,1,1<sup>3,6</sup>,0<sup>2,7</sup>]-4-dodecene of the following formula (f) encompassed within the formula (e)

and ethylene. The Patent does not describe the content of the tetracyclododecene of the copolymer of Example 44. When it is calculated under the assumption that all of the tetracyclododecene charged was introduced into the polymer, the polymer contains polymerized units derived from about 2 mole% at most of the tetracyclododecene. U. S. Patent 3,494,897 does not at all describe specifically copolymers of ethylene with tetracyclododecenes other than the tetracyclo[6,2,1,13,6,02,7]-4-dodecene of formula (f).

Journal of Polymer Science: Polymer Physics Edition, volume 12, 1607-1618 (1974) discloses copolymers of ethylene and norbornene derivatives having dynamic mechanical properties. Table II of this document shows a copolymer of ethylene containing 1 mole% of polymerized units derived from the same compound as formula (f) (named octahydrodimethanonaphthalene in this document). Table IV thereof states that this copolymer has a beta-relaxation temperature of 15°C.

The copolymers described in these prior art references which contain only 2% at the most of octahydrodimethanonaphthalene have a glass transition temperature of about 15°C at the highest. They strongly exhibit a rubbery nature and have poor heat resistance and mechanical properties.

U. S. Patent Application Serial No. 696,161 (European Laid-Open Patent Application No. 0156464) discloses a random copolymer composed of ethylene, a 1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene and optionally an alpha-olefin having at least 3 carbon atoms or a cycloolefin, wherein the mole ratio of polymerized units from the 1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene to polymerized units from ethylene is from 9:97 to 95: 5 and the 1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene is incorporated in the polymer chain as polymerized units without rino-opening.

The specification of U. S. Patent No. 2,883,372 discloses a normally solid copolymer of ethylene and 2,3-dihydrodicyclopentadiene having the following formula

said copolymer having a density in the range of 0.96 to 1.02 and being capable of being compression-molded at elevated temperatures into tough films.

The present invention seeks to provide a copolymer having excellent transparency, thermal resistance, heat aging resistance, chemical resistance, solvent resistance, dielectric properties and mechanical properties.

Accordingly the present invention provides a random copolymer which is transparent and is characterized in that

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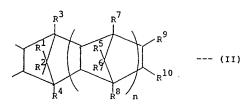
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(A) the copolymer comprises polymerized units from ethylene and polymerized units of at least one cycloolefin represented by the following formula (I)

wherein  $\rm R^1, R^2, R^3, R^4, R^5, R^6, R^7$  and  $\rm R^6$  are identical or different and each represents a hydrogen atom, halogen atom or a hydrocarbon group having 1 to 10 carbon atoms, and  $\rm R^9$  and  $\rm R^{10}$  are identical or different and each represents a hydrogen atom, a halogen atom or a hydrocarbon group having 1 to 10 carbon atoms or  $\rm R^9$  and  $\rm R^{10}$  are bonded to each other to form a group of the following formula

$$(R^{11} - C - R^{12})_{g}$$

in which  $\rm R^{11}$  and  $\rm R^{12}$  are identical or different and each represents a hydrogen atom, a halogen atom or a hydrocarbon group having 1 to 10 carbon atoms, and  $\ell$  is an integer of 3 or 4, and n is a positive integer of 1 to 3, (3) the mole ratio of the polymerized cycloolefin units to the polymerized ethylene units is from 3.97 to 60:40, (C) the or each cycloolefin of formula (f) is incorporated in the polymer chain as polymerized units represented by the following formula (f))



wherein all symbols are as defined above,

- (D) the copolymer has an intrinsic viscosity [η], measured in decalin at 135°C, of 0.01 to 20 dl/g,
- (E) the copolymer has a molecular weight distribution (Mw/Mn), measured by gel permeation chromatography, of not more than 4,
- (F) the copolymer has a crystallinity, measured by X-ray diffractometry, of 0 to 10%, and
- (G) the copolymer has a glass transition temperature (Tg) of 10 to 240°C as measured by a Dynamic Mechanical Analyzer.

The present invention also provides a process for producing a random copolymer as defined above, which process comprises continuously copolymerizing ethylene with the or each cyclooletin represented by formula (I) in a hydrocarbon medium in the presence of a catalyst formed from a vanadium compound soluble in the hydrocarbon medium and an organoaluminum compound while maintaining the atomic ratio of aluminum atoms to vanadium atoms in the reaction

system, Al:V, at 2 or more:1.

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The present invention additionally provides a process for preparing a modified random copolymer, which process comprises grafting on to a random copolymer, as defined above, 0.1 to 50 parts by weight of a monomer selected from (a) alpha, beta-unsaturated carboxylic acids and/or their derivatives, (b) styrenes, (c) organic silicon compounds having an olefinically unsaturated bond and a hydrolyzable group, and (d) unsaturated epoxy monomers per 100 parts by weight of the said random copolymer.

The present invention further provides molded articles prepared from a random copolymer as defined above or from a modified random copolymer prepared by a process as defined above.

The present invention also provides a modified random copolymer which obtainable by a process as defined above. In formula (I), R1, R2, R3, R4, R5, R6, R7 and R8 are identical or different, and each represents a hydrogen atom, a halogen atom or a hydrocarbon group having 1 to 10 carbon atoms. The halogen atom is, for example, fluorine, chlorine or bromine. The hydrocarbon group is preferably an alkyl group. Preferably the alkyl group has 1 to 5 carbon atoms. The alkyl group may be linear or branched, and includes, for example, methyl, ethyl, n-propyl, isopropyl, n-butyl, iso-butyl, t-butyl, pentyl, hexyl, heptyl, octyl, nonyl and decyl.

Examples of the halogen atom and the hydrocarbon group represented by  $\mathsf{R}^9$  and  $\mathsf{R}^{10}$  are the same as those given above.

The integer n is preferably 1 or 2. Examples of the cycloolefin of formula (I) include

20 1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2-methyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2-ethyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2-propyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2-hexyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 25 2-stearyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2,3-dimethyl-1,4,5,8 dimethano-1,2,3,4,4a,-5,8,8a-octahydronaphthalene, 2-methyl-3-ethyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2-chloro-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2-bromo-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 30 2-fluoro-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2,3-dichloro-1,4,5,8-dimethano-1,2,3,4,4a,-5,8,8a-octahydronaphthalene, 2-cyclohexyl-1,3,5,8,-dimethano-1,2,3,4,4a,-5,8,8a-octahydronaphthalene, 2-n-butyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 2-isobutyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene, 35 5,10-dimethyltetracyc1o[4,4,0,12.5,17.10]-3-dodecene, 2,10-dimethyltetracyclo[4,4,0,12.5,17.10] -3-dodecene, 11,12-diwethyltetracyc1o[4,4,0,12.5,17.10]-3-dodecene. 2,7,9-trimethyltetracyclo[4,4,0,13.5,17.10]-3-dodecene. 9-ethyl-2,7-dimethyltetracyclo[4,4,0,12.5, 17.10]-3-dodecene. 40 9-isobutyl-2,7-dimethyltetracyclo-[4,4,0,12.5,19.10]-3-dodecene, 9,11,12-trimethyltetracyclo[4,4,0,12.5,17.10]-3-dodecene, 9-ethyl-11,12-dimethyltetracyclo[4,4,0,12.5, 17,10]-3-dodecene. 9-isobutyl-11,12-dimethyl-3-tetracyclo-[4,4,0,12.5,17.10]-3-dodecene. 5,8,9,10-tetramethyltetracyc1ol4,4,0,12.5, 17.10] -3-dodecene, hexacyclo[6,6,1,13.6,110.13,02.7,09.14]-4-heptadecene, 45 12-methylhexacyclo[6,6,1,13,6,110,13,02,7,09,14]-4-heptadecene, 12-ethylhexacyclo[6,6,13.6,110.13,03.7,09.14]-4-heptadecene. 12-isobutylhexacyclo[6,6,1,13.6,110.13,O2.7, 09.14]-4-heptadecene, 1,6,10-trimethyl-12-isobutylhexacyclo[6,6,1, 13.6,110.13,02.7,09.14]-4-heptadecene. 50 octacyclo[8,8,12.9,14.7,111.19,113.16,0,03.8, 012.17]-5-dococene. 15-methyloctacyclo[8,8,12.9,14.7,111.18,113.16, 0,03.8,012.17]-5-dococene. 15-ethyloctacyclo[8,8,12.9,14.7,111.18,113.18, 113.16,0,03.8,012.17]-5-dococene, 1,3-dimethylpentacyclo[6,6,1,13,6,02.7,09,14]-4-hexadecene. 1,6-dimethylpentacyclo[6,6,1,13.6,02.7,09.14]-4-hexadecene 55 15,16-dimethylpentacyclo[6,6,1,13,6,02,7,09,14]-4-hexadecene. pentacyclo[6,5,1,13,6,02,7,09,13]-4-pentadecene, 1,3-dimethylpentacyclo[6,5,1,13,6,02,7,09,13]-4-pentadecene. 1,6-dimethylpentacyclof6.5, 1, 13.6, 02.7, 09.13]-4-pentadecene.

14,15-dimethylpentacyclo[6,5,1,13.6,02.7,09.13]-4-pentadecene, pentacyclo[6,6,1,13.6,02.7,09.14]-4-hexadecene, heptacyclo[6,7,12.8,14.7,111.7,0,03.6,012.16]-5-eicosene, and pentacyclo[6,8,12.9,14.7,111.18,0,03.8,012.17]-5-heneicosene.

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The compounds of formula (I) may be used singly or in combination.

The compounds of formula (I) can be easily produced by condensing cyclopentadienes with the corresponding olefins by the Diels-Alder reaction.

According to the process of this invention, the cycloolefin of formula (I) is copolymerized continuously with ethylene in a hydrocarbon medium in the presence of a catalyst. The catalyst is one formed from a soluble vanadium compound and an organoaluminum compound. In the copolymerization reaction carried out continuously, the atomic ratio of aluminum atoms to vanadium atoms, A1/V, is maintained at at least 2.

The soluble vanadium compound used in the process of this invention as a component of the catalyst is a vanadium compound soluble in the hydrocarbon medium in the polymerization reaction system. It may include vanadium compounds of formula  $VO(OR)_a X_b$  or  $V(OR)_b X_b$  wherein R is a hydrocarbon group such as an aliphatic, alicyclic or aromatic hydrocarbon group having 1 to 20 carbon atoms, preferably an aliphatic hydrocarbon group having 1 to 5 carbon atoms, especially 1 to 3 carbon atoms,  $0 \le a \le 3$ ,  $0 \le b \le 3$ ,  $2 \le a + b \le 3$ ,  $0 \le c \le 4$ ,  $0 \le c + d \le 4$ , and X is halogen such as CI, Br or I and adducts of these compounds with electron donors. Specific examples are  $VOCl_3$ ,  $VO(OCH_3)Cl_2$ ,  $VO(OCH_3)Cl_2$ ,  $VO(OCH_3)$ ,  $VO(OCH_3)Cl_3$ ,  $VO(OCH_3)$ ,

Compounds having at least one Al-C-bond in the molecule can be used as the organoaluminum compound used as a catalyst component. Examples are

(i) organoaluminum compounds of formula

wherein R¹³ and R¹⁴ are identical or different and each represents a hydrocarbon group having 1 to 15 carbon atoms, preferably 1 to 4 carbon atoms, X represents a halogen atom such as Cl, Br or l, m is a number represented by 0≦n≤3, 1 is a number represented by 0≦1<3, p is a number represented by 0≤1<3, and q is a number represented by 0≤4<3, provided that m+1+p+q=3.

(ii) Complex alkylated compounds of metals of Group I of the periodic table and aluminum of formula

wherein M1 is Li, Na or K, and R15 is as defined above.

Examples of the organialuminum compounds (i) are compounds of formula

wherein R13 and R14 are as defined above and m is preferably a number represented by 1.5≤m≤3, compounds of formula

wherein R<sup>13</sup> is as defined above, X is halogen such as CI, Br or I, and m is preferably 0<m<3, compounds of formula

wherein  $\mathsf{R}^{13}$  is as defined above and m is preferably a number represented by  $2 \leq \mathsf{m} < 3$ , and compounds of formula

wherein R13 and R14 are as defined above, X is halogen such as CI, Br or I,  $0 < m \le 3$ , and  $0 \le q < 3$ , provided that m + n + q = 3.

Examples of the aluminum compounds (i) include trialkyl aluminums such as triethyl aluminum, triisopropyl aluminum and tributyl aluminum; dialkyl aluminum alkoxides such as diethyl aluminum ethoxide and dibutyl aluminum bu-

toxide; alkyl aluminum sesquialkoxides such as ethyl aluminum sesquiethoxide and butyl aluminum sesquibutoxide; partially alkoxylated alkyl aluminums having the average composition of  $\mathrm{R}_{0.5}^1\mathrm{A}(\mathrm{OR}^2)_{0.5}$ ; partially halogenated alkyl aluminum halides such as diethyl aluminum chloride, dibutyl aluminum chloride and diethyl aluminum bromide, alkyl aluminum sesquiihalides such as ethyl aluminum sesquiihalides such as ethyl aluminum sesquiihoride and ethyl aluminum sesquiihalides such as ethyl aluminum sesquiihoride, partially hydrogenated alkyl aluminum, for example dialkyl aluminum dibhoride and butyl aluminum dibromide; partially hydrogenated alkyl aluminums, for example dialkyl aluminum hydrides such as distyl aluminum hydride and dibutyl aluminum hydride, and alkyl aluminum dibrogram such as ethyl aluminum dibrogram dibrogram aluminum such as ethyl aluminum ethoxychloride, butyl aluminum butoxychloride and ethyl aluminum aluminum ethoxybromide. As compounds similar to (1), organoaluminum compounds having at least two aluminums bonded through an oxygen or nitrogen atom may also be used. Examples of such compounds are  $(C_2H_5)_2\mathrm{AlOAl}(C_2H_5)_2$ ,  $(C_4H_9)_2\mathrm{AlOAl}(C_4H_9)_2$ , and  $(C_2H_5)_2\mathrm{AlOAl}(C_2H_5)_2$ .

Examples of the compounds (ii) are LiAl(C2H5)4 and LiAl(C7H15)4

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Among these, the aikyl aluminum halides, aikyl aluminum dihalides and mixtures of these are especially preferred. The copolymerization reaction in accordance with the process of this invention is carried out in a hydrocarbon medium. Examples of the solvent include aliphatic hydrocarbons having 5 to 15 carbon atoms such as pentane, hexane, heptane, octane and kerosene; alicyclic hydrocarbons having 5 to 15 carbon atoms such as cyclopentane, cyclohexane and methylcyclohexane; and aromatic hydrocarbons having 6 to 15 carbon atoms such as benzene, tolluene and xylene. These solvents may be used singly or in combination.

In the process of this invention, the copolymerization reaction is carried out continuously. During the reaction, the ratio of aluminum atoms to vanadium atoms, Al:V, is maintained at 2 or more:1, preferably 2 to 50:1, especially preferably 3 to 20:1.

The soluble vanadium compound and the organoaluminum compound are fed to the reaction system usually after dilution with the hydrocarbon medium. The concentration of the vanadium compound to be fed to the polymerization reaction system is usually not more than 10 times, preferably 7 to 1 times, more preferably 5 to 1 times, that in the polymerization reaction system. On the other hand, the organoaluminum compound may be fed to the polymerization system after its concentration is adjusted to not more than 50 times that in the polymerization system. In the process of this invention, the concentration of the soluble vanadium compound in the copolymerization reaction system is usually 0.01 to 5 gram-atoms/liter, preferably 0.05 to 3 gram-atoms/liter, as vanadium atoms. In the process of this invention for producing the cycloolefin random copolymer, the copolymerization reaction may be carried out in the copresence of an electron donor in the polymerization reaction system in addition to the soluble vanadium compound and the organoaluminum compound as catalyst ingredients. Examples of the electron donor include oxygen-containing electron donors such as alcohols, phenols, ketones, aldehydes, carboxylic acids, esters of organic acids or inorganic acids, ethers, acid amides, acid anhydrides and alkoxysilanes, and nitrogen-containing electron donors such as ammonia, amines, nitriles and isocyanates. The copolymerization reaction is carried out usually at -50 to 100°C, preferably -30 to 80°C, more preferably -20 to 60°C. The average residence time in the copolymerization reaction differs depending upon the type of the polymerization material, the concentrations of the catalyst components, and the polymerization temperature. Usually it is 5 minutes to 5 hours, preferably 10 minutes to 3 hours. The pressure during the copolymerization reaction is usually more than 0 to 50 kg/cm<sup>2</sup>, preferably more than 0 to 20 kg/cm<sup>2</sup>. If desired, it is carried out in the presence of an inert gas such as nitrogen or argon. To control the molecular weight of the copolymer, a molecular weight controlling agent such as hydrogen may be present in the reaction system. The polymerization reaction mixture after the copolymerization is treated in accordance with conventional methods to give the desired cycloolefin random copolymer.

The mole ratio of ethylene:cycloolefin fed to the copolymerization reaction system in the process of this invention is usually from 99:1 to 1:99, preferably 98:2 to 2:98.

In this invention, the cycloolefin is copolymerized with ethylene. As required, another copolymerized unsaturated monomer within a range which does not impair the objects of the invention, for example in an amount of 50 mole%, preferably 40 mole%, based on the ethylene units in the copolymer may be copolymerized in addition to these two essential components. Specific examples of the other copolymerizable unsaturated monomer include alpha-olefins having 3 to 20 carbon atoms such as propylene, 1-butiene, 4-methyl-1-pentene, 1-hexene, 1-decene, 1-decene, 1-tetradecene, 1-t

The copolymerization reaction in accordance with this invention can be advantageously carried out by continuously

feeding ethylene, the cycloolefin, and optionally the other copolymerizable component as materials to be polymerized, the soluble vanadium compound and organoaluminum compound as catalyst components, and the hydrocarbon medium into the polymerization system, and continuously withdrawing the polymerization reaction mixture from the polymerization reaction system.

According to the continuous process of this invention, a random copolymer having a narrow molecular weight distribution and good transparency can be produced.

The resulting copolymer solution continuously withdrawn from the polymerization reaction system is a hydrocarbon medium solution of the random copolymer. The concentration of the random copolymer in the resulting copolymer solution is usually 2.0 to 20.0% by weight, preferably 2.0 to 10.0% by weight. Contacting the resulting copolymer solution with a ketone or alcohol gives a precipitate of the random copolymer. The precipitate is separated by such separating means as filtration or centrifugal separation to give the random copolymer of this invention. The proportion of the ketone or alcohol used is usually 200 to 1,000 parts by weight, preferably 300 to 500 parts by weight, per 100 parts by weight of the resulting copolymer solution. Examples of the kelones are those having 3 to 7 carbon atoms such as acetone, methyl ethyl ketone, diethyl ketone, methyl isobutyl ketone, dipropyl ketone and acetylacetone. Examples of the alcohols are alcohols having 1 to 4 carbon atoms such as methanol, ethanol, propanol, isopropanol, butanol, sec-butanol and tert-butanol. The ketones or alcohols may contain a small amount of water. The use of a mixture of the ketone or alcohol with usually 0.1 to 10% by weight, preferably 1 to 5% by weight, of water is suitable since it gives a copolymer powder having low contents of the unreacted cycloolefin monomer and a low-molecularweight polymer and high bulk density. Contacting of the resulting copolymer solution with the ketone or alcohol is carried out with stirring at a temperature of usually 0 to 100°C, preferably 10 to 70°C, especially preferably at a temperature near the boiling point of the ketone or alcohol. This is effected by using a vessel-type mixer having agitating vanes such as turbine blades and comb blades. The rotating speed of the blades is usually 200 to 2,000 rpm, preferably 800 to 1,500 rpm.

As a result of the after-treatment described above, the random copolymer is precipitated usually in powder form to form a suspension. The suspension containing the copolymer is separated into the copolymer and the mother liquor by such a separating means as centrifugation or filtration. The separated copolymer is further extracted with a ketone to give a random copolymer having low contents of the unreacted cycloolegifin monomer and a low-molecular-weight polymer, a narrow molecular weight distribution, an arrow composition distribution, and a high glass transition temperature. The proportion of the ketone used in the extraction is such that the concentration of the copolymer in the ketone is usually 10 to 100 g/liter, preferably 30 to 60 g/liter. The temperature at which the copolymer is contacted with the ketone is usually 10 to 85°C, preferably 15 to 80°C. The contacting treatment between the copolymer and the ketone is usually carried out with stirring using, for example, a vessel-type mixer having agitating blades such as turbine blades and comb blades. The rotating speed of the blades at this time is usually 50 to 400 rpm, preferably 100 to 200 rpm. The time required for contacting is usually 1 to 8 hours, preferably 2 to 5 hours. Examples of the ketone may be the same as those examplified for the ketone used for the precipitation treatment. The copolymer which has been contacted with the ketone may be separated by separated dy separating means such as centrifugation or filtration. As required, the separated copolymer is further washed with the ketone. The washing conditions may be the same as the ketone contacting treatment conditions described above.

The random copolymer of this invention obtained by the above after treatment usually has a bulk density of 0.05 to 0.3, preferably 0.1 to 0.25, and is easy to handle at the time of molding. Furthermore, since the copolymer of this invention has low contents of the unreacted cycloolofin monomer and a low-molecular-weight polymer, optical materials, particularly optical memory discs, molded from it permit reduction of noise caused by, for example, reflection.

Thus, the present invention gives a random copolymer in which the mole ratio of polymerized cycloolefin of formula (I) units to polymerized ethylene units is from 3:97 to 60:40, preferably from 5:95 to 50:50.

The random copolymer of this invention has an intrinsic viscosity [ $\eta$ ], measured in decalin at 135°C, of 0.01 to 20 d/ $\eta$ , preferably 0.05 to 10 d/ $\eta$ .

The random copolymer of this invention has a molecular weight distribution (Mw/Mn), measured by gel permeation chromatography (GPC), of not more than 4, preferably not more than 3.5 especially preferably not more than 3. The random copolymer of this invention is characterized in that this molecular weight distribution is narrow. This means that the random copolymer of this invention has a low content of a low-molecular-weight polymer. Accordingly, when the random copolymer of this invention is molded into an optical material such as an optical memory disc or optical fibers, the optical material has good surface smoothness, low surface tack, or good mechanical properties and is suitable for optical applications.

The random copolymer of this invention has a crystallinity, measured by X-ray diffractometry, of 0 to 10%, preferably 0 to 8%, especially preferably 0 to 7%. The advantage of the copolymer having a crystallinity of 10% or below is that when it is molded into an optical material such as an optical memory disc or optical fibers, noise of the optical material caused by, for example, refraction or diffused reflection is reduced

The copolymer has a Tg of 10 to 240°C, more preferably 20 to 200°C.

The random copolymers of this invention are molded by known methods. For example, they can be extrusion-molded, injection-molded, blow-molded, or rotationally molded by using, for example, a vent-type extruder, a twin-screw extruder, a Cokneader, a platicator, a mixtruder, a twin conical screw extruder, a planetary screw extruder, a gear-type extruder or a screwless extruder, in the molding process, known additives such as heat stabilizers, light stabilizers, antistatic agents, slip agents, antiblocking agents, antibaze agents, lubricants, inorganic and organic fillers, dyes and pigments may be used as required.

Phenolic or sulfur-type antioxidants may be cited as examples of such additives. The phenolic antioxidants include, for example, phenols such as 2,6-di-tert-butyl-p-cresol, stearyl (3,3-dimethyl-4-hydroxybenzyl)thioglycolate, stearyl beta-(4-hydroxy-3,5-di-tert-butyl-4-hydroxybenzyl)phosphate, 2,4-6-fris(3,5-di-tert-butyl-4-hydroxybenzyl)phosphate, 2,4-6-fris(3,5-di-tert-butyl-4-hydroxybenzyl)phosphate, 2,2-methyl-enebis(4-methyl-6-tert-butyl-phenol), 2,2-methyl-enebis(6-tert-butyl-phenol), 2,2-methyl-enebis(6-tert-butyl-phenol), 2,2-methyl-enebis(6-tert-butyl-phenol), 2,2-methyl-enebis(6-tert-butyl-phenol), 2,2-methyl-enebis(6-tert-butyl-phenol), 1,1,3-tris(3,5-bis[4-hydroxy-3-tert-butyl-phenyl)butene, bis[2-tert-butyl-4-methyl-6-(2-hydroxy-3-tert-butyl-5-methylbenzyl)phenyl)] terephthalate, 1,3,5-tris(2,6-di-methyl-3-hydroxy-4-tert-butyl-4-hydroxy-bert-butyl-4-hydroxy-1,3,5-triazine and 4,4-thiobis (6-tert-butyl-m-cresol), and polyhydric phenol/carbonic acid oligoesters such as carbonic acid oligoesters (for example, having a degree of polymerization of 2, 3, 4, 5, 6, 7, 8, 9, 10) of 4,4-butylidenebis(2-tert-butyl-5-methylphenol).

Examples of the sultur-type antioxidant include dialkyl thiodipropionates such as dilauryl, dimyristyl or distearyl thiodipropionate, and esters (such as pantaerythrifol tetralaurythiopropionate) formed between alkylthiopropionic acids such as butyl, octyl-, lauryl- or stearylthiopropionic acid and polyhydric alcohols (such as glycerol, trimethylolethane, trimethylopropane, pentaerythrifol or tris-hydroxyethyl diisocyanurate).

Phosphorous-containing compounds may also be incorporated. Examples include tricctyl phosphite, trilauryl phosphite, tridecyl phosphite, ctyldiphenyl) phosphite, tris(2.4-di-tert-butylphenyl) phosphite, triphenyl phosphite, tris(butoxyethyl) phosphite, tris(novlphenyl) phosphite, itsicanyl pentaerythritol diphosphite, tetra-(tridecyl)-1,1,3-tris(2-methyl-5-tert-butyl-4-hydroxy-phenyl) phosphite, tetra-(tridecyl)-4,4'-botylidenebis(3-methyl-6-tert-butylphenol) diphosphite, tris(3.5-di-tert-butyl-4-hydroxyphenyl) phosphite, tris(16-di-tert-butyl-4-hydroxyphenyl) phosphite, tris(16-di-tert-butyl-4-repthyl-6-tert-butylphenol) fighosphite, tris(3.5-di-tert-butyl-4-hydroxyphenyl) phosphite, tris(19-di-tert-butyl-19-entaerythritol diphosphite, bis(2.6-di-tert-butyl-19-entaerythritol diphosphite, bis(2.6-di-tert-butyl-4-methylphenyl)) pentaerythritol diphosphite, tris(4,4'-isopropylidenebis(2-tert-butyl-19-entaerythritol diphosphite, tris(4,4'-isopropylidenebis(2-tert-butyl-19-entaerythritol diphosphite, tris(4,4'-isopropylidenebis(2-tert-butyl-19-entaerythritol diphosphite, tris(4,4'-isopropylidenebis(2-tert-butyl-19-entaerythritol diphosphite, tris(1,3-di-stear-oyloxyisopropyl) phosphite, tris(4,4'-isopropylidenebis(2-tert-butyl-19-entaerythritol diphosphite, tris(1,3-di-stear-oyloxyisopropyl) phosphite, tris(1,3-di-stear-oyloxyisopropyl) p

There can also be used 6-hydroxycoumarone derivatives such as alpha-, beta-, gamma- and delta-tocopherols and mixtures thereof, a 2,5-dimethyl-substitution product, 2,5,8-trimethyl-substituted product or 2,5,7,8-tetramethyl-substituted product or 2,5,7,8-tetramethyl-substituted product or 2,4-methyl-pent-3-eny)-6-hydroxycoumarone, 2,2,7-trimethyl-5-tert-butyl-6-hydroxycoumarone, 2,2,5-trimethyl-6-tert-butyl-6-hydroxycoumarone, and 2,2-dimethyl-5-tert-butyl-6-hydroxycoumarone.

It is also possible to incorporate a compound represented by the general formula

$$M_xAI_y(OH)_{2x+3y-2z}(A)_z.aH_2O$$

wherein M represents Mg, Ca or Zn, A is an anion other than a hydroxyl anion, x, y and z are positive numbers, and a represents 0 or a positive number.

Examples of the compounds of the above formula are

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$$\begin{split} &\text{Zn}_{6}\text{Al}_{2}(\text{OH})_{16}\text{CO}_{3}\text{ 4H}_{2}\text{O},\\ &\text{Zn}_{6}\text{Al}_{2}(\text{OH})_{1}\text{6SO}_{4}\text{ 4H}_{2}\text{O},\\ &\text{Mg}_{8}\text{Al}_{2}(\text{OH})_{16}\text{SO}_{4}\text{ 4H}_{2}\text{O}, \end{split}$$

and

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There may also be added an antioxidant having a 2-benzofuranone skeleton, such as 3-phenyl-2-benzofuranone and 3-phenyl-4,6-di-1-butyl-2-benzofuranone as disclosed in the specification of Japanese Laid-Open Patent Publication No. 501,181/1980.

Examples of the light stabilizers include hydroxybenzophenones such as 2-hydroxy-4-methoxybenzophenone, 2-hydroxy-4-n-octoxybenzophenone, 2,2'-dihydroxy-4-methoxybenzophenone and 2,4-dihydroxy-3,5-di-ten-butyl-phenyl)-5-chlorobenzotriazole, 2-(2'-hydroxy-3',5'-di-ten-butyl-phenyl)-5-chlorobenzotriazole, 2-(2'-hydroxy-3',5'-di-ten-butyl-phenyl)-5-chlorobenzotriazole, 2-(2'-hydroxy-3',5'-di-ten-butyl-phenyl)-5-chlorobenzotriazole, 2-(2'-hydroxy-3',5'-di-ten-butyl-phenyl)-5-chlorobenzotriazole, 2-(2'-hydroxy-3',5-di-ten-butyl-4-hydroxybenzote, inckel salt and (3,5-di-ten-butyl-4-hydroxybenzote, inckel salt and (3,5-di-ten-butyl-4-hydroxybenzote, inckel salt and (3,5-di-ten-butyl-4-hydroxybenzote)-phenol)-nickel salt and (3,5-di-ten-butyl-4-hydroxybenzyl)-phosphonic acid monoethyl ester nickel salt is ubstituted acryloniriles such as methyl alpha-cyano-beta-methyl-beta-(p-methoxyphenyl)-acrylate; oxalic acid diamide and N-2-ethylphenyl-N-2-ethoxyphenyl-oxalic acid diamide; and hinderal mine compounds such as bis(2,2,6,6-tetramethyl-4-piperidine)sebacate, poly[(6-(1,1,3,3-tetramethylbutyl)imino)-1,3,5-triazine-2,4-diyl 4-(2,2,6,6-tetramethyl-1-piperidine)betanethylene] and a condensation product of dimethyl succinate and 2-(4-hydroxy-2,2,6,6-tetramethyl-1-piperidine)betanethylene)

Examples of the lubricants include aliphatic hydrocarbons such as paraffin wax, polyethylene wax and polypropylene wax; higher fatty acids such as capric acid, lauric acid, myristic acid, palmitic acid, margaric acid, stearic acid, arachidic acid and behenic acid: metal salts of higher fatty acids such as lithium, calcium, sodium, magnesium and potassium salts of the above-exemplified fatty acids; aliphatic alcoholes such as palmityl alcohol, celyl alcohol and stearyl alcohol; aliphatic arnides such as caproic amide, caprylic amide, carpric amide, lauric amide, myristic amide, palmitic amide and stearic amide; esters formed between fatty acids and alcohols; and fluorine compounds such as fluoroalkylcarboxylic acids metal salts thereof, and metal salts of fluoroalkyl-sulfonic acids.

Examples of the fillers include inorganic or organic fibrous fillers such as glass fibres, silver- or aluminum-coated glass fibers, stainless steel fibers, aluminum fibers, potassium titanate fibers, carbon fibers, whiskers, Kevlar® fibers and superhigh elastic polyethylene fibers; and inorganic or organic powdery, granular or flaky fillers such as talc, calcium carbonate, magnesium hydroxide, calcium oxide, magnesium sulfate, graphite, nickel powder, silver powder, copper powder, carbon black, silver-coated glass beads, aluminum-coated glass beads, aluminum flakes, stainless steel flakes and nickel-coated graphite.

The random copolymers of this invention have excellent transparency, heat resistance, heat aging resistance, chemical resistance, solvent resistance, dielectric properties and mechanical properties, a narrow and uniform molecular weight distribution, and a narrow and uniform composition distribution. Accordingly, those having a low molecular weight are synthetic waxes and are useful as cancles, impregnating agents for metches, paper finishing agents, sizes, antioxidants for rubber, waterproofing agents for cardboards, slow releasing agents for chemical fertilizers, heat accumulators, binders for ceramics, paper condensers, electric insulating materials for electric wires and cables, agents for decelerating neutrons, fiber finishing aids, water-repellents for building materials, protecting agents for coatings, polishing agents, thixotropy imparting agents, core hardening agents for pencils and crayons, carbon ink substrates, electrophotographic toners, lubricants and releasing agents for molding of synthetic resins, resin coloring agents, hot-mell adhesives, and lubricant greases. Those having a high molecular weight can be used in an optical field as optical lenses, optical discs, optical fibers and windowpanes, in an electrical field as a water tank for electrical irons, parts of electronic overs, base boards for liquid crystal display, base boards for printed circuit boards, high frequency circuit boards and transparent electrically conductive sheets or films, in medical and chemical fields as syninges, pipettes and animal gages, and in other various fields as housings of measuring instruments, and helmets.

When the copolymers of this invention have a glass transition temperature (Tg) below 100°C, they can be used in a field utilizing their shape memory, and as a vibration controlling material or a tube. Specifically, they can be used as joints for irregularly-shaped pipes, laminating agents for the interior and exterior parts of pipes and rods, clamping pins for optical fiber connectors, plaster casts, containers, automobile bumpers, various space eliminating materials, vibration controlling materials or sound insulating materials in the form of a laminate with a metal surface material, and tubes for use in medical therapy.

The random copolymers of this invention may be used as a blend with various known polymers. Examples of such known polymers are:

(A) Polymers derived from hydrocarbons having 1 or 2 unsaturated bonds

Polyolefins, such as polyethylene, polypropylene, polyisobutylene, poly(methylbutene-1), poly(4-methylpentene-1), poly(methylbutene-1), polyisoprene, polybutadiene and polystyrene, or crosslinked products thereof.

Copolymers of the monomers constituting the above polymers with each other, such as ethylene/propylene copolymer, propylene/butene-1 copolymer, propylene/isobutylene copolymer, styrene/isobutylene copolymer, terpolymers of ethylene, propylene and dienes such as hexadiene, bicyclopentadiene and 5-ethylidene-2-norbornene, and terpolymers of ethylene, butene-1 and dienes such as hexadiene, dicyclopentadiene and 5-ethylidene-2-norborne.

Blends, grafted polymers, and block copolymers of these polymers may also be cited.

(B) Halogen-containing vinyl polymers

Polyvinyl chloride, polyvinylidene chloride, polyvinyl fluoride, polychloroprene, and chlorinated rubbers.

(C) Polymers derived from alpha, beta-unsaturated carboxylic acids or the derivatives thereof Polyacrylate, polymethacrylate, polyacrylamide, and polyacrylonitrile.

Copolymers of the monomers constituting the above-exemplified polymers with other copolymerizable monomers, such as acrylonitrile/butadiene/styrene copolymer, acrylonitrile/styrene copolymer, and acrylonitrile/styrene/acrylate copolymer.

(D) Polymers derived from unsaturated alcohols, amines, acyl derivatives thereof, or acetals

Polyvinyl alcohol, polyvinyl acetate, polyvinyl stearate, polyvinyl benzoate, polyvinyl maleate, polyvinyl butyral, polyallyl phthalate and polyallylmelamine.

Copolymers of the monomers constituting the above-exemplified polymers with other copolymerizable monomers, such as ethylene/vinyl acetate copolymer.

(E) Polymers derived from epoxides

Polyethylene oxide and polymer derived from bisglycidyl ether.

(F) Polyacetals

Polyoxymethylene, polyoxyethylene, and polyoxymethylene containing ethylene oxide.

- 35 (G) Polyphenylene oxide
  - (H) polycarbonate
- (i) Polysulfone

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- (J) Polyurethane and urea resins
- (K) Polyamides and copolyamides derived from diamines and dicarboxylic acids and/or aminocarboxylic acids or the corresponding lactams

Nylon 6, nylon 66, nylon 11, and nylon 12.

- (L) Polyamide-polyethers
- (M) Polyesters derived from dicarboxylic acids and dialcohols and/or hydroxycarboxylic acids or the corresponding lactones

Polyethylene terephthalate, polybutylene terephthalate and poly(1,4-dimethylolcyclohexane terephthalate).

- (N) Crosslinked polymers derived from aldehydes and phenols, urea or melamine Phenol/formaldehyde resin, urea/formaldehyde resin, and melamine/formaldehyde resin.
- (O) Alkyd resinsGlycerin/phthalic acid resin.

(P) Unsaturated polyester resins derived from copolyesters of saturated and unsaturated dicarboxylic acids and polyhydric alcohols using vinyl compounds as crosslinking agents, and halogen-containing modified resins thereof.

### (Q) Natural polymers

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Cellulose, rubber and protein, or derivatives thereof, such as cellulose acetate, cellulose propionate, cellulose acetate and cellulose ether.

When the copolymers of this invention are used as synthetic waxes, they may, of course, be mixed with various known waxes.

The random copolymers of this invention may be used as a blend with each other.

The random copolymer of this invention may be modified by grafting thereto a monomer selected from the group consisting of (a) alpha, beta-unsaturated carboxylic acids and/or their derivatives, (b) styrenes, (c) organic silicon compounds having an olefinic unsaturated bond and a hydrolyzable group and (d) unsaturated epoxy compounds. The modified random copolymer obtained has the same excellent properties as the random copolymer of the invention and also especially good adhesion to metals and synthetic resins and good compatibility with other resins. The amount of the grafting monomer in the modified random copolymer is 0,1 to 50 parts by weight, preferably 0.5 to 35% by weight, per 100 parts by weight of the random copolymer of the invention. The modified random copolymer usually has an intrinsic viscosity [ $\eta$ ] of 0.03 to 20 dl/g, preferably 0.05 to 5 dl/g.

Examples of the grafting monomer are:

Examples of the unsaturared carboxylic acids and their derivatives (a) include unsaturated carboxylic acids such as acrylic acid, interacrylic acid, alpha-ethylacrylic acid, maleic acid, fumaric acid, itaconic acid, citraconic acid, tetrahydrophthalic acid, methyltetrahydrophthalic acid, endocis-bicyclo[2,2,1]-hept-5-ene-2,3-dicarboxylic acid (methyllhadic acid®), and methylendocis-bicyclo[2,2,1]-hept-5-ene-2,3-dicarboxylic acid (methyllhadic acid®), and their halides, amides, imides, anhydrides and esters. Specific examples of these derivatives are malenyl chloride, maleinuc anhydride, citraconic anhydride, monomethyl maleate and dimethyl maleate. Of these, the unsaturated dicarboxylic acids or their anhydrides are preferred. Maleic acid, Nadic acid or their anhydrides are especially preferred.

Examples of the styrenes (b) are compounds represented by the following formula

$$R^{20} C = C R^{21}$$

wherein H<sup>20</sup>, H<sup>21</sup> and H<sup>22</sup> each represent a hydrogen atom or a lower alkyl group. Specific examples are styrene, alpha-methylstyrene, o-methylstyrene, m-methylstyrene, p-methylstyrene, m-ethylstyrene, p-ethylstyrene, o-iso-propylstyrene, m-isopropylstyrene and p-isopropylstyrene. Of these, styrene, m-methylstyrene and p-methylstyrene are preferred.

Examples of the organic silicon compound (c) having an olefinic unsaturated bond and a hydrolyzable group are compounds represented by the following formula

$$R^{23}R^{24}SiY^{1}Y^{2}$$

wherein H23 and H24 are identical or different and each represents a monovalent group composed of carbon, hydrogen and optionally oxygen and having an olefinically unsaturated bond, and Y1 and Y2 are identical or different and each represents a hydrolyzable group, compounds of the following formula

wherein  $\mathsf{R}^{23}$  is as defined, and  $\mathsf{Y}^1, \mathsf{Y}^2$  and  $\mathsf{Y}^3$  are identical and different and each represents a hydrolyzable group, and compounds of the following formula

wherein  $\mathsf{R}^{23},\,\mathsf{Y}^1$  and  $\mathsf{Y}^2$  are as defined above, and X represents an organic group free from an olefinic unsaturated

Examples of R<sup>23</sup> and R<sup>24</sup> are vinyl allyl, butenyl, cyclohexenyl, cyclopentadienyl,  $CH_2=C(CH_3)COO(CH_2)_3$ .  $CH_2=C(CH_3)COO(CH_2)_2$ . Of these, the hydrocarthylic of the cyclopentadienyl  $CH_2$  is the hydrocarthylic of the cyclopentadien  $CH_2$  in  $CH_2$  is the cyclopentadien  $CH_2$  in  $CH_2$  in C

bon groups having a terminal olefinically unsaturated bond and esters thereof are preferred. The vinyl group is especially preferred.

Examples of Y¹, Y² and Y³ are alkoxy groups such as methoxy, ethoxy, butoxy and methoxyethoxy, acyloxy groups such as formyloxy, acetoxy and propionoxy, oxime groups such as  $-ON=C(CH_0)_2$ ,  $-ON=CHCH_2C_2H_3$  and  $-ON=C(C_6H_5)_2$ , and substituted amino groups and arylamino groups such as  $-ON+CH_3$ ,  $-ON+CH_3$ , and  $-ON+CH_3$ , and  $-ON+CH_3$ , and  $-ON+CH_3$ ,  $-ON+CH_3$ , and  $-ON+CH_3$ , and -

Examples of X in the above formula include methyl, ethyl, propyl, tetradecyl, octadecyl, phenyl, benzyl and tolyl. Of these, monovalent hydrocarbon groups are preferred.

Organic silicon compounds preferably used in this invention are those of the second formula given above, particularly those in which the groups Y1, Y2 and Y3 are identical. Especially preferred are vinyltriatkoxysilanes, vinyltriethoxysilane, vinyltriethoxysilane, vinyltriethoxysilane, vinyltriethoxysilane, vinyltriethoxysilane, vinyltriethoxysilane, vinyltriethoxysilane, vinyltriethoxysilane.

The unsaturated epoxy monomers (d) are preferably monomers having at least one polymerizable unsaturated bond and at least one epoxy group per molecule. Examples include unsaturated glycidyl esters represented by the following general formula

wherein R<sup>25</sup> represents a hydrocarbon group having a polymerizable ethylenically unsaturated bond,

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unsaturated glycidyl ethers represented by the general formula

wherein  $\mathsf{R}^{25}$  is as defined above, and Z represents a divalent group of the formula -CH2-O- or

**√**⊙-•-•

and epoxyalkenes represented by he general formula

R<sup>26</sup>-CH<sub>2</sub>

wherein R25 is as defined, and R26 represents a hydrogen atom or a methyl group.

Specific examples of the monomers (d) are glycidyl acrylate, glycidyl methacrylate, mono- and di-glycidyl itaconate, mono-, di- and-liriglycidyl butene-tricarboxylates, mono- and di-glycidyl citraconates, mono- and di-glycidyl endo-cis-bicyclo[2.2.1]-hept-5-ene-2-methyl-2.9-di-carboxylates, mono- and di-glycidyl endo-cis-bicyclo[2.2.1]-hept-5-ene-2-methyl-2.9-di-carboxylates, mono-and di-glycidyl allylsuccinates, glycidyl psytyene-carboxylate, allyl glycidyl ether, 2-methylalkyl glycidyl ether, styrene p-glycidyl ether, 3.4-epoxy-1-butene, 3.4-epoxy-1-butene, 3.4-epoxy-1-pentene, and vinylcyclohexene monoxide. Of these, glycidyl acrylate and glycidyl methacrylate are preferred.

The modified random copolymer may be produced by various known methods. For example, the random copolymer is melted, and the grafting monomer is added and graft-copolymerized. Alternatively, the random copolymer is dissolved in a solvent, and the grafting monomer is added and graft-copolymerized. In either case, the reaction is preferably carried out in the presence of a radical initiator in order to perform graft copolymerization efficiently. The radical initiator may include organic peroxides, organic peresters and azo compounds. Ionizing radiations and ultraviolet light may also be used to generate radicals.

The modified random copolymer obtained by the above procedure has excellent heat resistance as shown by its high glass transition temperature which is one measure of heat resistance. Specifically, the modified random copolymer usually has a glass transition temperature, measured by a Dynamic Mechanical Analyzer (DMA), of 20 to 250°C, in many cases 30 to 220°C. The modified random copolymer also usually has a softening temperature of 20 to 230°C, in many cases 30 to 200°C. The softening temperature is defined as the temperature at which a quart needle (diameter

0.635 mm) penetrates 0.1 mm into the copolymer under a load of 49 g when the temperature is elevated at a rate of 5°C/min, using TMS (thermomechanical analyzer, a product of E. I. du Pont de Nemours & Co.).

The modified copolymer usually has a density, determined by the method of ASTM D 1505, of 0.95 to 1.20 g/cm $^3$ , in many cases 0.96 to 1.10 g/cm $^3$ .

When the random copolymer of this invention is crosslinked with sulfur or organic peroxides or by actinic light such as electron beams or radioactive rays, its heat resistance, chemical resistance, solvent resistance and mechanical properties can be further improved.

The properties of the cycloolefin random copolymers obtained in this invention were measured in accordance with the following method.

(1) Copolymer composition (mole%)

On the basis of the cycloolefin unit content of the random copolymer determined by 13°-NMR (200 MHz), a calibration curve is prepared between the cycloolefin unit content and the height of the peak of an absorption band based on the cycloolefin unit determined by infrared spectroscopy. The peak height of the absorption band of the infrared absorption spectrum of the random copolymer is measured, and the cycloolefin unit content is calculated. The ethylene unit content of the random copolymer is calculated by subtracting the cycloolefin unit content from the entire units.

(2) Intrinsic viscosity [n]

Measured at 135°C using a Ubbelohde viscometer.

(3) Glass transition temperature (Tg)

Measured by a Dynamic Mechanical Analyzer (DMA, made by E. I. du Pont de Nemours & Co.).

(4) Crystallinity

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Determined by X-ray diffractometry.

(5) Volatile component (VM)

A weight change was measured under the conditions of 300°C, 1 torr and 1 hour.

(6) Content of the unreacted cycloolefin

The polymer was dissolved in cyclohexane, and the amount of the unreacted cycloolefin was measured by gas chromatography.

(7) Molecular weight distribution

The molecular weight distribution (Mw/Mn) is determined in the following manner in accordance with the procedure described at pages 14-114 of "Gel Permeation chromatography" by Takeuchi, published on May 20, 1976 by Maruzen Co., Ltd., Tokyo.

(1) Using standard polystyrene of a known molecular-weight (mono-dispersed polystyrene, a product of Toyo Soda Mfg. Co., Ltd., Japan), the molecular weight M of the polystyrene sample and its GPC (gel permeation chromatography) count are measured. A calibration curve for the molecular weight M and the EV (elution volume) is drawn. The concentration of the polymer at this time is set at 0.02% by weight.

(2) A gel permeation chromatogram of the sample is taken by the GPC measuring method, and the number average molecular weight (Mn =  $\frac{\Sigma M |N|}{\Sigma N_i}$ ) and the weight average molecular weight (Mw =  $\frac{\Sigma M^2 N_i}{\Sigma N_i}$ ) are calculated for copolymer

by (1) above, and the value (Mw/Mn) is determined.

The sample is prepared under the following conditions, and the conditions for GPC are as shown below.

# Preparation of the sample

- (a) The sample is taken into an Erlenmeyer flask together with o-dichlorobenzene so as to provide a 0.02% solution.
- (b) Into the Erlenmeyer flask containing the sample is added 0.1% by weight, based on the polymer solution, of 2,6-di-tert, butyl-p-cresol as an antioxidant.
- (c) The Erlenmeyer is heated to 140°C, and the contents are stirred for about 30 minutes to dissolve the polymer and the antioxidant.
- (d) Then, at 135 to 140°C, the solution is filtered by a 1η Millipoere filter.
- (e) The filtrate is subjected to gel permeation chromatography.

# Conditions for gel permeation chromatography

(a) Device: Model 150C, made by Waters Company

- (b) Column: TSK-GMH6 (mix type) made by Toyo Soda Mfg. Co., Ltd.
- (c) Amount of the sample: 500 µl
- (d) Temperature: 140°C
- (e) Flow rate: 1 ml/min.
  5 (f) Total theoretical stage
  - (f) Total theoretical stages of the column;

# 1 x 104 to 4 x 104 (measured with acetone)

The following Examples further illustrate the present invention.

### 10 EXAMPLE 1

Ethylene and 1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphthalene [Table 1, (a): abbreviated as DMON] were copolymerized in a 2-liter polymerization reactor equipped with agitating blades.

The polymerization reactor was continuously charged at its top with a cyclohexane solution of DMON at a rate of 0.4 liter/hour so as to provide a DMON concentration of 60 g/liter in the polymerization reactor, a cyclohexane solution of VO(OC, Hs)Cl, as a catalyst at a rate of 0.7 liter/hour so as to provide a vanadium concentration of 0.7 mmole/liter in the polymerization reactor (the concentration of vanadium fed at this time was 2.86 times that in the polymerization reactor), a cyclohexane solution of ethyl aluminum sesquichloride as a catalyst at a rate of 0.4 liters/hour so as to provide an aluminum concentration of 5.6 mmoles/liter in the polymerization reactor, and 0.5 liters/hr of cyclohexane. In the mean-time, the polymerization mixture in the polymerization reactor was withdrawn continuously from the bottom of the polymerization reactor so that the amount of the polymerization mixture in the reactor was always kept at 1 liter. Furthermore, 80 liters/hr of ethylene, 80 titers/hr of nitrogen and 0.2 liter/hr of hydrogen were fed from the top of the polymerization reactor. The copolymerization was carried out at 10°C by circulating a cooling medium into a jacket fitted to the exterior portion of the reactor. As a result of the copolymerization reaction under the above conditions, a polymerization reaction mixture containing the ethylene/DMON random copolymer was obtained. A mixture of cyclohexane and isopropanol (1:1) was added to the polymer solution with drawn from the bottom of the polymerization reactor to stop the polymerization reactor. Thereafter, an aqueous solution composed of 1 liter of water and 5 ml of concentrated hydrochloric acid and the polymer solution were contacted at a ratio of 1:1 with strong stirring by a homomixer to transfer the catalyst residue to the aqueous layer. The mixture was left to stand, and the water layer was removed. The residue was washed twice with distilled water to purify and separate the polymer solution. The polymer solution was contacted with 3 times its amount of acetone with strong stirring, and the solid portion was collected by filtration and fully washed with acetone. Thereafter, the resulting solid portion was put into acetone in a concentration of 40 g/ liter, and reacted at 60°C for 2 hours. The solid portion was then collected by filtration, and dried in a stream of nitrogen at 130°C and 350 mmHg for 24 hours.

By the above procedure, the ethylene/DMON copolymer was obtained at a rate of 94 g/hr. The copolymer had an ethylene content of 61.3 mole%, an intrinsic viscosity of 0.85, an Mw/Mn, determined by GPC, of 2.50, a crystallinity, determined by X-ray diffractometry, of 0%, and a glass transition temperature (Tg) of 143°C. The copolymer contained 0.4% by weight of volatile comonents and 0.13% by weight of the unreacted monomers.

# 40 EXAMPLES 2-14

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Example 1 was repeated except that the copolymerization conditions indicated in Table 2 were used. The properties of the resulting copolymers are shown in Table 3.

Table 1

		Cycloolefin
(a)		1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydro- naphthalene
(p)	C2H5	2-ethyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octa- hydronaphthalene
(c)	CH <sub>3</sub>	2,3-dimethyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a- octahydronaphthalene
(g)	CH <sub>3</sub>	2-methyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a- octahydronaphthalene
(e)	CH <sub>3</sub>	12-methylhexacyclo[6,6,1,1 <sup>3,6</sup> ,1 <sup>10,13</sup> ,0 <sup>2,7</sup> ,0 <sup>9,14</sup> ].

EP 0 203 799 B1

		Polymer-	tempera- turg ( C)	10		
		Amount of hir-		0.2	30 0.2 0.2 0.2	
		Amount	ethylene fed (1/hr)	80	110 110 150 150 150	
		punoc	Concentration in the reactor (mmol/2)	5.6	2.7.0.00	
Table 2	Copolymerization conditions	Aluminum compound	Name	A1(C <sub>2</sub> H <sub>5</sub> ) <sub>1.5</sub> Cl <sub>1.5</sub>	A1(C <sub>2</sub> H <sub>5</sub> ) <sub>1,5</sub> C <sub>1,5</sub> / A2(C <sub>2</sub> H <sub>5</sub> ) <sub>1,5</sub> C <sub>1,5</sub> / A1(C <sub>2</sub> H <sub>5</sub> ) d1 <sub>2</sub> (7/3)	iters/hr.
	olymeriza	punođu	Concentration in the reactor (mmol/!)	0.7		was 50 1
	ďo	Vanadium compound	Name	vo(cc <sub>2</sub> H <sub>5</sub> ) c1 <sub>2</sub>	voc <sub>1</sub> 2,012	The amount of nitrogen fed was 50 liters/hr. Nitrogen was not fed. Table 4
		Cycloolefin*3)	Concentration in the reactor (9/1)	09	**************************************	The amount of nitroge Nitrogen was not fed. Table 4
		1	Name	Table 1	(£) (£) (£) (£) (£) (£) (£) (£) (£) (£)	*1): TE *2): N: *3): TE
	- X	n Toling		7	2 3 4 4 5 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6 6	

			T														
5			Amount of the residual monomer (wt%)	0.13	0.12	0.12	0.12	0.13	0.21	0.12	0.11	0.15	0.11	0.14	0.11	0.10	0.12
			VM (wt8)	0.4	0.5	0.4	0.5	0.5	9.0	0.5	0.3	9.0	0.5	0.5	0.2	0.3	0.4
15		the copolymer	Ãw∕Ān	2.5	2.3	5.6	2.4	2.7	2.9	2.3	3.0	2.7	2.5	2.4	3.0	2.9	2.4
20		of the co	<sup>DM8-Т9</sup> (С)	143	135	140	147	127	155	152	131	137	92	79	45	160	145
25	Table 3	Properties o	Crystal- linity (%)	0	0	0	0	0	0	0	0	0	0	0	0	0	0
30		Pro	["]	0.85	0.82	0.83	0.84	0.93	0.57	0.89	0.31	0.70	0.84	0.50	0.76	0.71	0.67
35			<pre>Ethylene content (mol%)</pre>	61.3	64.8	63.2	64.0	70.2	9.79	61.2	67.2	60.3	83.7	82.9	93.4	56.7	58.0
40 45			Amount of the copolymer (g/hr)	104	96	94	102	122	84	78	120	06	102	100	130	96	106
50		Example		٦	7	m	4	ທ	9	7	8	σ.	10	11	12.27	13	14

# EXAMPLE 15

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Using a 2-liter glass polymerization reactor equipped with agitating blades, ethylene and 2-methyl-1,4,5,8-dimethano-1,2,3,4,4a,5,8,8a-octahydronaphtahlene (to be abbreviated as M-DMON; (d) of Table 1 were copolymerized continuously.

Specifically, the reactor was charged at its top with 0.9 liter/hr of a toluene solution of M-DMON so as to provide an M-DMON concentration in the reactor of 60 g/liter, 0.7 liter/hr of a toluene solution of VO(CC<sub>2</sub>H<sub>5</sub>)Cl<sub>2</sub> as a catalyst so as to provide a vanadium concentration in the reactor of 0.5 mmole/liter, and 0.4 liter/hr of a toluene solution of whyly aluminum sesquichloride as a catalyst so as to provide an aluminum concentration in the reactor of 2 mmoles/liter. In the meantime, the polymer solution was continuously withdrawn from the bottom of the reactor so that the amount of the polymer solution in the reactor was maintained always at 1 liter. Furthermore, 35 liters/hr of ethylene and 80 liters/hr of nitrogen were fed from the top of the reactor. The copolymerization reaction was carried out at 10°C by circulating a cooling medium through a jacket fitted to the outside of the reactor. As a result of performing the copolymerization under the aforesaid conditions, a polymerization reaction mixture containing an ethylene/M-DMON random copolymer was obtained. A small amount of methanol was added to the polymer solution withdrawn from the bottom of the reactor to stop the copolymerization reaction. The polymer solution was then put into a large amount of acetone/methanol to precipitate the resulting copolymer. The copolymer was fully washed with acetone and dried under reduced pressure for one day at 80°C. By the above operation, the ethylen/M-DMON random copolymer was obtained at a rate of 60 g/hour.

The copolymer was found to have an ethylene content of 63 mole%. The copolymer had an intrinsic viscosity, measured in decalin at 135°C, of 0.92, an iodine number of 1.0, a crystallinity, determined by X-ray diffractometry, of 0%, and a transparency, determined by a haze meter on a 1 mm sheet sample in accordance with ASTM D 1003-52, x 2 1%.

The glass transition temperature Tg of the copolymer, determined from the peak temperature of the loss modulus E" which was measured at a temperature elevation rate of 5°C/min. by a dynamic mechanizal analyzer was 127°C. Its melting point Tm was measured within a temperature range of -120 to 400°C by DSC (Du Pont 990 type) at a temperature elevation rate of 10°C/min.). No melting curve (peak) was observed.

# EXAMPLES 16-24 AND COMPARATIVE EXAMPLE 1

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Example 15 was repeated except that the copolymerization conditions shown in Tables 4 and 5 were used. The properties of the resulting copolymers are shown in Table 5. In Example 22, a 1:1 mixture of toluene and cyclohexane was used as the polymerization solvent.

EP 0 203 799 B1

Table 4

				1000		
Cycloolefin	olefin		Ca	Catalyst		
			Vanadium compound	punodwo	Aluminum compound	put
Name Concentration in the reactor (g/t)	Concentration in the reactor (g/%)		Name	Concentration in the reactor (mmol/%)	Name	Concentration in the reactor (mmol/s)
Table 1 60 (d)	09		VO(0C2H5)C12	0.5	A1 (C2H5)1.5C11.5	2.0
	t			=		
			ı	-	=	
	*		=	8.0	•	6.4
:	:		VOC13	:	•	=
9		->	VO(OC, H5) C1,	0.5		4.0
(p) (q)			1	8.0		6.4
; (c)				E		•
(a)	E			:	=	*
(e)				F	=	
(p)	09			8.0		8.0
		- 1				

EP 0 203 799 B1

Tahle 5

		,										
	₩/Mn	2.5	2.8	3.6	2.8	2.9	2.7	2.8	3.0	2.9	2.5	ı
	DSC-13m (°C)	,	ı	ı	ı	,	92	1	1	ı	1	1
lymer	DW8-T9 (C)	127	118	107	116	115	34	113	111	115	131	ı
е соро	Haze (%)	3.1	2.7	2.0	2.2	2.3	4.5	2.6	2.3	2.4	2.8	ı
Properties of the copolymer	Iodine Crystal- value linity (%)	0	0	0	0	0	0	0	0	0	0	1
Proper	Iodine value	1.0	6.0	6.0	0.7	6.0	1.0	6.0	8.0	6.0	1.0	ı
	[h]	0.92	1.21	1.40	1.25	1.23	2.94	1.18	1.20	1.21	0.95	1
	Ethylene content (mole%)	63	99	72	89	<b>L9</b>	94	29	99	65	69	i
Amount of the	copolymer yielded (4/hr)	09	94	140	106	92	64	96	98	95	78	trace
	tempera- turg ( <sup>C</sup> C)	10				=	30	70			:	10
	ethylene fed (t/hr)	35	09	100	09	=	98	09	:			99
Ex- ample		15	16	17	18	19	70	21	77	73	24	Comp. Ex. 1

### **EXAMPLE 25**

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Fifty grams of the ethylene/DMON random co-polymer (A) obtained in Example 1 was dissolved in 500 ml of xylene at 125°C in a nitrogen atmosphere in a glass reactor. Then, a xylene soilution of maleic anhydride (abbreviafted as MAH) (12 g/30 ml) and a xylene solution of dicumyl peroxide (abbreviated as DCP) (0.27 g/30 ml) were ted gradually over a period of 4 hours from separate lines into the reactor.

Since MAH had low solubilty in xylene, it was dissolved by heating with an infrared lamp, and the heating was continued until its feeding was terminated.

After the feeding, the reaction was continued for 2 hours, and after the reaction, the reaction solution was cooled to room temperature. The reaction solution was put into a large amount of acetone to precipitate the polymer. The resulting gratted ethylene/DMON copolymer was filtered, repeatedly washed with acetone, and dried under reduced pressure at 80°C for 1 day to give the desired MAH-grafted ethylene/DMON copolymer. The amount of MAH grafted, measured by oxygen analysis of the modified copolymer was 1,13 by weight. The modified copolymer had an intrinsic viscosity, measured in decalin at 135°C, of 0.86 dl/g, a density, determined in accordance with ASTM D 1505, of 1.025 g/cm³, a glass transition temperature (Tg) of 145°C.

### **EXAMPLES 26 & 27**

Example 25 was repeated except that 50 g of each of the cycloolefin random copolymers indicated in Table 6 was used instead of the ethylene/DMON random copolymer, and the grafting conditions were changed as in Table 6. The results are shown in Table 7.

#### Table 6

Example	Random copolymer	Grafting o	conditions	
		MAH (g/30 ml)	DCP (g/30 ml)	
26	Α	12	0.27	
27	В	12	0.27	
	ained in Example 1, tained in Example 4, a	nd		

# Table 7

Example	Propertie	s of the	modified copolymer	
	Amount of MAH grafted (wt.%)	[ŋ]	Tg (by DMA method)	Density (g/cm <sup>3</sup> )
26	1.13	0.86	145	1.025
27	1.23	0.86	149	1.023

# EXAMPLES 28-30

Example 25 was repeated except that the random copolymer, grafting monomer and the radical initiator were changed as shown in Table 8. The results are shown in Table 9.

### Table 8

Example	Random copolymer	Amount (g)	Grafting monomer	Amount (g)	DCP (g)
28	A	50	а	20	0.33
29	D	50	b	16	0.34
30	E	50	С	10	0.27

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### Table 8 (continued)

				on a cay		
Ì	Example	Random copolymer	Amount (g)	Grafting monomer	Amount (g)	DCP (g)
-	A: Obt	tained in Example 1,				
ļ	D: ob	stained in Example 2, a	ind			
		otained in Example 3 nyl-tri-ethoxy silane				
ı	b: sty	rene				
[	C: gly	ycidyl methacrylate				

Table Q

Example	Properties of	of the mo	odified copolymer	
	Amount of grafted monomer (wt.%)	[η]	Tg (by DMA method)	Density (g/cm³)
28	0.25	0.87	144	1.026
29	1.34	0.86	138	1.021
30	1.13	0.85	142	1.023

### Claims

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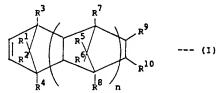
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# 1. A random copolymer which is transparent and is characterized in that

(A) the copolymer comprises polymerized units of ethylene and polymerized units of at least one cycloolefin represented by the following formula (I)



wherein R<sup>1</sup>, R<sup>2</sup>, R<sup>3</sup>, R<sup>4</sup>, R<sup>5</sup>, R<sup>6</sup>, R<sup>7</sup> and R<sup>8</sup> are identical or different and each represents a hydrogen atom, halogen atom or a hydrocarbon group having 1 to 10 carbon atoms, and R<sup>9</sup> and R<sup>10</sup> are identical or different and each represents a hydrogen atom, a halogen atom or a hydrocarbon group having 1 to 10 carbon atoms or R<sup>9</sup> and R<sup>10</sup> are bonded to each other to form a group of the following formula

$$(R^{11} - C - R^{12})_{g}$$

in which  $R^{11}$  and  $R^{12}$  are identical or different and each represents a hydrogen atom, a halogen atom or a hydrocarbon group having 1 to 10 carbon atoms, and  $\ell$  is an integer of 3 or 4, and n is a positive integer of 1 to 3 (B) the mole ratio of the polymerized cyclooletin units to the polymerized ethylene units is from 3.97 to 60:40, (C) the or each cyclooletin of formula (I) is incorporated in the polymer chain as polymerized units represented by the following formula (II)

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- wherein all symbols are as defined above, (D) the copolymer has an intrinsic viscosity  $[\eta]$ , measured in decalin at 135°C, of 0.01 to 20 dl/g,
- (E) the copolymer has a molecular weight distribution (Mw/Mn), measured by gel permeation chromatography, of not more than 4,
- (F) the copolymer has a crystallinity, measured by X-ray diffractometry, of 0 to 10%, and
- (G) the copolymer has a glass transition temperature (Tg) of 10 to 240°C as measured by a Dynamic Mechanical Analyzer.
- A random copolymer according to claim 1 wherein the mole ratio (B) of the polymerized cycloolefin units to the
  polymerized ethylene units is from 5:95 to 50:50.
  - 3. A random copolymer according to claim 1 or 2 which has a glass transition temperature (Tg) of 20 to 200°C.
- 4. A process for producing a random copolymer as defined in any one of the preceding claims, which process comprises continuously copolymerizing ethylene with the or each cycloolefin represented by formula (1) in a hydrocarbon medium in the presence of a catalyst formed from a vanadium compound soluble in the hydrocarbon medium and an organo-aluminum compound whille maintaining the atomic ratio of aluminum atoms to vanadium atoms in the reaction system, A1:V, at 2 or more:1.
  - A process according to claim 4 wherein the soluble vanadium compound is added to the reaction system in a concentration not more than 10 times its existing concentration in the reaction system in order to maintain the atomic ratio A1:V at 2 or more:1.
- 35 6. A process for preparing a modified random copolymer, which process comprises grafting on to a random copolymer, as defined in any one of claims 1 to 4, 0.1 to 50 parts by weight of a monomer selected from (a) alpha, beta-unsaturated carboxylic acids and/or their derivatives, (b) styrenes, (c) organic silicon compounds having an olefinically unsaturated bond and a hydrolyzable group, and (d) unsaturated epoxy monomers per 100 parts by weight of the said random copolymer.
  - Molded articles prepared from a random copolymer as defined in any one of claims 1 to 4 or from a modified random copolymer prepared by a process as claimed in claim 6
  - 8. A modified random copolymer which is obtainable by a process as defined in claim 6.

### Patentansprüche

- 1. Ein statistisches Copolymer, das transparent ist und dadurch gekennzeichnet ist, daß
  - (A) das Copolymer polymerisierte Einheiten von Ethylen und polymerisierte Einheiten von wenigstens einem Cycloolefin umfaßt, das durch die folgende Formel (I) dargestellt ist

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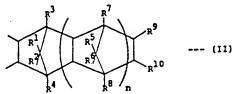
$$\begin{array}{c|c}
R^{3} & R^{7} \\
\hline
R^{5} & R^{6} \\
\hline
R^{4} & R^{8} & R^{10}
\end{array}$$

worin R¹, R², R³, R⁴, R⁵, R⁶, R² und R⁶ gleich oder verschieden voneinander sind und jeweils ein Wasserstoffatom, Halogenatom oder eine Kohlenwasserstoffgruppe mit 1 bis 10 Kohlenstoffatomen darstellt und R⁶ und R¹⁰ gleich oder verschieden voneinander sind und joweils ein Wasserstoffatom, ein Halogenatom oder eine Kohlenwasserstoffgruppe mit 1 bis 10 Kohlenstoffatomen darstellen oder Rð und R¹⁰ miteinander verbunden sind, um eine Gruppe der folgenden Formel

$$(R^{11} - C - R^{12})_{i}$$

zu bilden, worin  $\mathbb{R}^{11}$  und  $\mathbb{R}^{12}$  gleich oder verschieden voneinander sind und jeweils ein Wasserstoffatorn, ein Halogenatom oder eine Kohlenwasserstoffgruppe mit 1 bis 10 Kohlenstoffatornen darstellen und 1 eine ganze Zahl von 3 bis 4 ist und n einen positive ganze Zahl von 1 bis 3 ist;

- (B) das Molverhältnis der polymerisierten Cycloolefineinheiten zu den polymerisierten Ethyleneinheiten von 3:97 bis 60:40 beträgt;
- (C) das oder jedes Cycloolefin der Formel (I) in die Polymerkette als polymerisierte Einheiten eingebracht sind, welche durch die folgende Formel (II) dargestellt sind



worin alle Symbole die oben angegebene Bedeutung besitzen,

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- (D) das Copolymer eine in Decalin bei 135°C gemessene intrinsiche Viskosität ( $\eta$ ) von einschließlich 0,01 bis 20 dl/g besitzt,
- (E) das Copolymer eine durch Gelpermeationschromatographie gemessene Molekulargewichtsverteilung (Mw/Mn) von nicht mehr als 4 besitzt,
- (F) das Copolymer eine durch Röntgenbeugung gemessene Kristallinität von einschließlich 0 bis 10 % besitzt und
- (G) das Copolymer eine mit einem dynamischen mechanischen Analysator gemessene Glasübergangstemperatur (Tg) von 10 bis 240°C besitzt.
- Statistisches Copolymer nach Anspruch 1, wobei das Molverh
  ältnis (B) der polymerisierten Cycloclefineinheiten zu den polymerisierten Ethyleneinheiten zwischen einschließlich 5:95 bis 50:50 liegt.
  - 3. Statistisches Copolymer nach Anspruch 1 oder 2, das eine Glasübergangstemperatur (Tg) von 20 bis 200°C auf-

weist.

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- Ein Verfahren zur Herstellung eines wie in jedem der vorhergehenden Ansprüche definierten statistischen Copolymeres, wobei das Verfahren das kontinuierliche Copolymerisieren von Ethylen mit dem oder jedem Cycloolefin umfaßt, das durch die Formel (I) dargestellt ist, in einem Kohlenwasserstoffmedium in Gegenwart eines Katalysators, der aus einer in dem Kohlenwasserstoffmedium löslichen Vanadiumverbindung und einer Organo-Aluminiumverbindung gebildet ist, währenddessen das Atomverhältnis von Aluminiumatomen zu Vandiumatomen Al:V in dem Reaktionssystem bei 2 oder mehr:1 gehalten wird.
- 5. Verfahren nach Anspruch 4, worin die lösliche Vanadiumverbindung dem Reaktionssystem in einer Konzentration 10 von nicht mehr als dem 10fachen seiner vorhandenen Konzentration in dem Reaktionssystem zugegeben wird, um das Atomverhältnis Al:V bei 2 oder mehr:1 zu halten.
  - 6. Verfahren zum Herstellen eines modifizierten statistischen Copolymeres, wobei das Verfahren, das Aufpfropfen auf ein wie in jedem der Ansprüche 1 bis 4 definiertes statistisches Copolymer von 0,1 bis 50 Gewichtsteile eines Monomeres pro 100 Gewichtsteile des statistischen Copolymeres umfaßt, das aus (a) α, β-ungesättigten Carbonsäuren und/oder deren Derviaten, (b) Styrolen, (c) organischen Siliconverbindungen mit einer olefinisch ungesättigten Bindung und einer hydrolisierbaren Gruppe und (d) ungesättigten Epoximonomeren ausgewählt ist.
- 20 7. Geformte Gegenstände, hergestellt aus einem wie in jedem der Ansprüche 1 bis 4 definierten statistischen Copolymer oder aus einem durch ein wie in Anspruch 6 beanspruchtes Verfahren hergestelltes modifiziertes statistisches Copolymer.
  - 8. Ein modifiziertes, statistisches Copolymer, das durch ein wie in Anspruch 6 definiertes Verfahren erhältlich ist.

### Revendications

1. Copolymère statistique transparent caractérisé en ce que

(A) le copolymère comporte des motifs polymérisés dérivés d'éthylène et des motifs polymérisés dérivés d'au moins une cyclooléfine représentée par la formule suivante (I)

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(I) 18

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dans laquelle  $R^1$ ,  $R^2$ ,  $R^3$ ,  $R^4$ ,  $R^5$ ,  $R^6$ ,  $R^7$  et  $R^8$ , identiques ou différents, représentent chacun un atome d'hydrogène, un atome d'halogène ou un groupe hydrocarbone comportant de 1 à 10 atomes de carbone, et R<sup>9</sup> et R<sup>10</sup>, identiques ou différents, représentent chacun un atome d'hydrogène, un atome d'halogène ou un groupe hydrocarboné comportant de 1 à 10 atomes de carbone, ou R9 et R10 sont liés l'un à l'autre pour former un groupe de formule

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$$(R^{11} - C - R^{12})_{\ell}$$

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dans laquelle  $R^{11}$  et  $R^{12}$ , identiques ou différents, représentent chacun un atome d'hydrogène, un atome d'halogène ou un groupe hydrocarboné comportant de 1 à 10 atomes de carbone, et 1 est un nombre entier égal à 3 ou 4, et n est un nombre entier positif compris entre 1 et 3;

(B) le rapport molaire des motifs polymérisés dérivés d'une cyclooléfine aux motifs polymérisés dérivés d'éthy-

lène est compris entre 3/97 et 60/40;

(C) la cyclooléfine ou chaque cyclooléfine de formule (I) est incorporée dans la chaîne du polymère sous forme de motifs polymérisés représentés par la formule suivante (!!)

(II)

dans laquelle tous les symboles sont définis ci-dessus;

- (D) le copolymère a une viscosité intrinsèque [η], mesurée dans la Décaline® à 135 °C, comprise entre 0,01 et 20 dì/g;
- (E) le copolymère a un indice de polydispersité (M<sub>o</sub>/M<sub>n</sub>), mesuré par chromatographie par perméation de gel, ne dépassant pas 4:
- (F) le copolymère a un taux de cristallinité, mesuré par diffraction de rayons X, compris entre 0 et 10 %,
- (G) le copolymère a une température de transition vitreuse, déterminée avec un appareil d'analyse mécanicodynamique, comprise entre 10 et 240 °C.
- 2. Copolymère statistique conforme à la revendication 1 dans lequel le rapport molaire (B) des motifs polymérisés 25 dérivés d'une cyclooléfine aux motifs polymérisés dérivés d'éthylène est compris entre 5/95 et 50/50.
  - Copolymère statistique conforme à la revendication 1 ou 2 ayant une température de transition vitreuse (T<sub>v</sub>) comprise entre 20 et 200 °C.
- 4. Procédé de préparation d'un copolymère statistique conforme à une quelconque des revendications précédentes, 30 lequel procédé comprend la copolymérisation en continu d'éthylène et de la ou de chaque cyclooléfine représentée par la formule (I), dans un milieu hydrocarboné en présence d'un catalyseur formé à partir d'un composé de vanadium soluble dans le milieu hydrocarboné et d'un composé organo aluminique, avec maintient du rapport des atomes d'aluminium aux atomes de vanadium AIV dans le système réactionnel à une valeur supérieure ou égale 35 à 2/1.
  - 5. Procédé conforme à la revendication 4 dans lequel on ajoute au système réactionnel le composé de vanadium soluble en une concentration n'excédant pas 10 lois sa concentration existant dans le système réactionnel afin de maintenir un rapport atomique Al/V supérieur ou égal à 2/1.
  - 6. Procédé de préparation d'un copolymère statistique modifié, lequel procédé comprend le greffage de 0,1 à 50 parties en poids, par rapport à 100 parties en poids dudit copolymère statistique, d'un monomère choisi parmi (a) les acides carboxyliques α,β-insaturés et/ou leurs dérivés, (b) les styrènes, (c) les composés organiques du silicium comportant une liaison à insaturation éthylénique et un groupe hydrolysable, et (d) des monomères insaturés à fonction époxyde, sur un copolymère statistique défini par une quelconque des revendications 1 à 4.
  - 7. Articles moulés préparés à partir d'un copolymère statistique conforme à une quelconque des revendications 1 à 4 ou à partir d'un copolymère statistique modifié préparé selon un procédé conforme à la revendication 6.
- 8. Copolymère statistique modifié pouvant être obtenu selon un procédé conforme à la revendication 6. 50

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